

# NATURAL REFRIGERANTS

## with high pressure compressors in Industrial plants

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### LINE-UP OF 'NATURAL 5'.

Mayekawa was founded in 1924 and is to-day one of the world's largest industrial refrigeration companies. It actively promotes the 'NATURAL 5' refrigerants, including ammonia, CO<sub>2</sub>, hydrocarbon gasses, air and water. Mayekawa is active in ammonia compressors for more than 85 years, for hydrocarbons and CO<sub>2</sub> for more than 40 years.

The 'NATURAL 5' refrigerants cover the full application range -100°C/+100°C from cryogenics, freezing, cooling, air conditioning up to heating.

Refrigerant (Natural Five)	NH <sub>3</sub> R-717	CO <sub>2</sub> R-744	HC Hydrocarbon	H <sub>2</sub> O R-718	Air R-728
80°C	Utility hot water Heating	Utility hot water			
60°C			Utility hot water Heating HVAC	Heat recovery	
10°C	Chilled water Ice making	Chilled water Ice making		Chiller	
-15°C	Cold storage, Freezer, Fish boat				
-25°C	Specific Refrigeration needs				
-40°C	Freezer, Freeze-dry, Super Low temp storage				
-50°C			Cryogenics		
-60°C					Cryogenics
-100°C					
Notes	• Conventional system • National Projects	• HeatCO <sub>2</sub> m	• Nat'l Proj. • Butane + Propane	• Nat'l Proj. • Adsorption • Heat recovery	• Nat'l Proj. • Air-cycle

As it is our tradition to bring as much as possible information from the field we have chosen this time for high pressure compressors in Industrial plants.

The need of higher pressure compressors is increasing with the new applications :

such as CO<sub>2</sub> refrigeration - including defrosting,

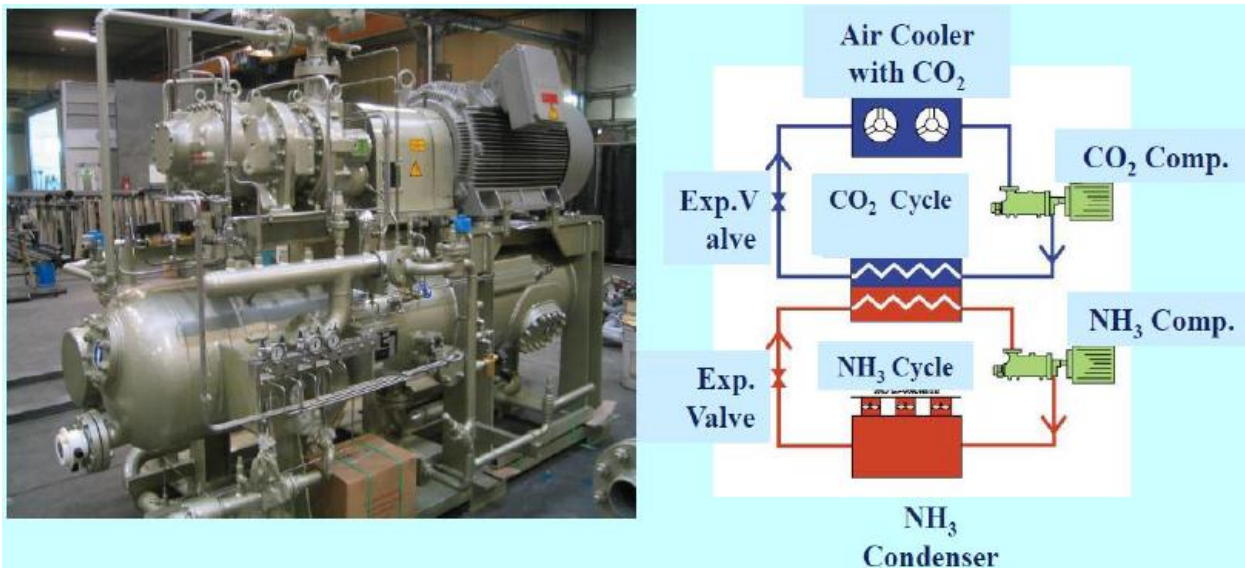
and the intensively expanding heat pump applications at higher output temperatures and capacities.

## CO<sub>2</sub>/NH<sub>3</sub> CASCADE COMPRESSION REFRIGERATION.

The field case of to-day is an industrial low temperature refrigeration plant using a CO<sub>2</sub>/NH<sub>3</sub> cascade system with CO<sub>2</sub>- and NH<sub>3</sub> compressors as is illustrated in the scheme.

The CO<sub>2</sub> cycle is shown on the top of the scheme with CO<sub>2</sub> compressors, -air cooler, expansion valve and cascade CO<sub>2</sub> condensor/NH<sub>3</sub> evaporator.

The NH<sub>3</sub> cycle is shown on the bottom.



The unit picture shows a 50 bar oil injected screw compressor typical for use with low temperature cooling (-40°C to -52°C with CO<sub>2</sub>) including also defrosting mode (+10°C at 45bar).

## FIELD CASE.

The plant belongs to an international group of companies active in traditional bakery products for bakeries, food service operations, supermarkets and industrial customers, installed by the contractor AXIMA REFRIGERATION GDF SUEZ in France.

## INTRO

The starting point for the plant was to realize a freezing plant for bakery products requiring  $-35^{\circ}\text{C}$  product temperatures for approx..3000kW to be realized in 2 phases.

The choice was made to apply for a  $\text{CO}_2/\text{NH}_3$  cascade which is a main trend for low temperature refrigeration in food industry where  $\text{CO}_2$  of  $-40^{\circ}\text{C}$ , still at very usefull pressure of 10 bara, to obtain  $-35^{\circ}\text{C}$  product temperature.

The  $\text{CO}_2$  is natural and can be used direct in the freezers.

$\text{CO}_2$  can also be used for defrosting of the freezers with the high pressure compressors

The high stage of the cascade can be done with the natural refrigerant  $\text{NH}_3$  with limited charge only for the high temperature side in the  $\text{NH}_3$  machineroom and condensors.

The realization of the plant was done in 2011 for phase 1 followed by phase 2 in 2013.

## EQUIPMENT



The table shows the overview of the installed compressors for the low temperature - and the high temperature side of the cascade plant.

The CO<sub>2</sub> evaporating temperature is kept at -40°C and the freezing is realized by using 6 compressors :

1 pce 50 bar screw compressor performing 741kW(-40°C) freezing and 606kW(+8°C) defrosting,

4 pieces 50 bar piston compressors performing 1196kW(-40°C) freezing(total) and 696kW (+8°C) defrosting (total).

1 piece 66bar piston compressor performing 940kW( -40°C) freezing.

All CO<sub>2</sub> compressors are condensing at -8°C, while the NH<sub>3</sub> compressor evaporate at -12°C with evaporative condensers designed at +35°C.

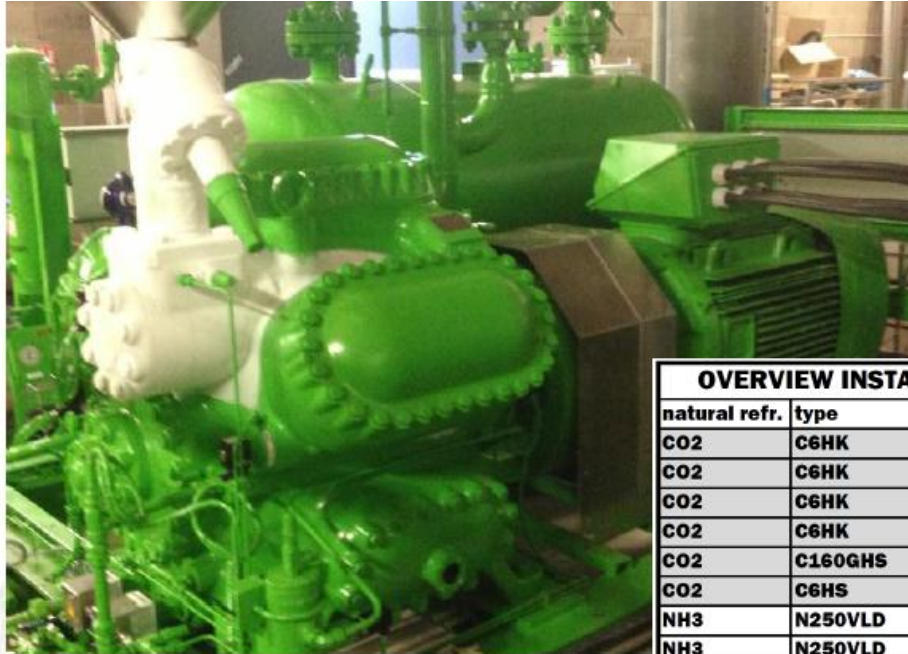
3 pieces 26 bar screw compressors performing 3502kW (-12°C) evaporating are taking the total heat rejection from all CO<sub>2</sub> compressors.

The picture shows the 50bar screw compressor freezing/defrosting (right side picture) and the 66 bar piston compressor.

All mentioned compressors are equipped with frequency drive convertors so that speeds can be reduced from maximum to minimum speed by keeping the highest

efficiency. This avoids that mechanical part loading needs to be done so that the highest COP's can be maintained.

The overview table shows the installed units with installation dates and the actual total number of operating hours for each machine.



<b>OVERVIEW INSTALLED COMPRESSORS :</b>				
<b>natural refr.</b>	<b>type</b>	<b>unit</b>	<b>date</b>	<b>hours</b>
<b>CO2</b>	<b>C6HK</b>	<b>C1</b>	<b>2011</b>	<b>7997</b>
<b>CO2</b>	<b>C6HK</b>	<b>C2</b>	<b>2011</b>	<b>1664</b>
<b>CO2</b>	<b>C6HK</b>	<b>C3</b>	<b>2011</b>	<b>5444</b>
<b>CO2</b>	<b>C6HK</b>	<b>C4</b>	<b>2011</b>	<b>877</b>
<b>CO2</b>	<b>C160GHS</b>	<b>C5</b>	<b>2011</b>	<b>71</b>
<b>CO2</b>	<b>C6HS</b>	<b>C6</b>	<b>2013</b>	<b>1871</b>
<b>NH3</b>	<b>N250VLD</b>	<b>CV1</b>	<b>2011</b>	<b>19895</b>
<b>NH3</b>	<b>N250VLD</b>	<b>CV2</b>	<b>2011</b>	<b>5107</b>
<b>NH3</b>	<b>N250VLD</b>	<b>CV3</b>	<b>2011</b>	<b>5603</b>

## EFFICIENCY ANALYSIS

An overview of the cascade plant COP-c is made based on the initial design conditions and compared to the average obtained operation.

The basis for the calculation is operation 24 hours per day, 5 days per week, 50 weeks on year basis at 80% plant load, what means 4800 hours per year.

The table shows the freezing capacities, absorbed power at the compressor shafts, total heat rejection and the corresponding coefficients of performance (COP-c)

For the low temperature CO<sub>2</sub> side and the high temperature NH<sub>3</sub> side.

For a design condensing temperature of 35°C the final COP of the cascade plant is 1,68.



## DESIGN

CO2/NH3 CASCADE		RT	BKW	THR	COPc-each	COPc-total
TE=-40°C	TC=+35°C	kW	kW	kW		
CO2 LS	C160GHS	741	200	941	3,7	
	C6HK	1196	289	1485	4,1	
	C6HS	940	212	1152	4,4	
	total	2877	701	3578	4,1	
NH3 HS	N250VLDx2	3502	1006		3,5	
	N250VLD					
<b>TOTAL</b>		<b>2877</b>	<b>1707</b>			<b>1,68</b>

## AVERAGE

CO2/NH3 CASCADE		RT	BKW	THR	COPc-each	COPc-total
TE=-40°C	TC=+29,5°C	kW	kW	kW		
CO2 LS	C160GHS	741	200	941	3,7	
	C6HK	1196	289	1485	4,1	
	C6HS	940	212	1152	4,4	
	total	2877	701	3578	4,1	
NH3 HS	N250VLDx2	3575	825		4,3	181 kW
	N250VLD					
<b>TOTAL</b>		<b>2877</b>	<b>1526</b>			<b>1,88</b> 12%

Based on the average condensing temperature of 29,5°C on year basis it is possible to reduce the power consumption on the NH3 high stage compressors by 181 kW per hours, which results in a total cascade plant COP-c of 1,88 which is 12% higher than design.

This 12% COP-c improvement represents a yearly saving of 4800 (hrs) x 181( kW) or 868.800 kWh. At an average electricity cost of 70 €cent per kWh this represents an energy saving amount of 608.160 € per year!

This electricity saving reflects also directly on the equivalent CO2 emmission saving.

## CONCLUSION

It is clear that natural refrigerants are the main trend for industrial refrigeration in food industry !

CO<sub>2</sub> proves its advantages with :

direct use in the freezing equipment

low temperature refrigeration at usefull pressures (-40°C 10bara)

defrosting mode operation availability (10°C 45bara, 20°C 58bara in f(compressor design)

design optimizing COP<sub>c</sub> 1,68->1,88 by applying lowest average condensing temperature 29,5°C, resulting in saving of 870 mW electricity per year or 608 k€/year.

Low energy consumption

Low CO<sub>2</sub> emmision

low cost (smaller size equipment)

less risc for food safety

cascade with minimized NH<sub>3</sub> charge

low insurance cost

## COMBINED NH3 CHILLER/HOT WATER HEAT PUMP.



The next system exists of a 2 stage NH3 compressor system mounted on 1 skid as a closed system.

The low stage is used as a water-chiller and the high stage, using a high pressure piston compressor, is used as an over-compression hot water heat pump.

The picture shows :

The low stage compressor with drive motor and discharge piping to the oil separator in the front on the left side.

The insulated suction line is visible on the left side of the compressor with the PHE evaporator and NH3 separator on the left in the back side.

The high stage compressor with drive motor and insulated discharge piping to the insulated oil separator on the front of the right side.

The with Armaflex insulated suction line connected to the heat source flash tank on the right side,

and the insulated discharge piping connected to the insulated condenser on the back side.



The table shows the compressor models with cooling/heating outputs, compressor shaft power inputs, the corresponding COP's.

<b>CHILLER</b>		
compressor model		piston N8M
cooling output water temperature	°C	1,5
capacity	kW	1000
bkw	kW	250
COP-c		4,0
<b>HOT WATER HEAT PUMP</b>		
compressor model		piston N6HS
heating output water temperature	°C	90
capacity	kW	1500
bkw	kW	250
COP-h		6,0
<b>COP-total</b>		<b>5,0</b>

The package produced 1000kW chilled water of 1,5°C (NH<sub>3</sub> evaporation at 0°C) and 1500kW hot water of 90°C (NH<sub>3</sub> condensing at +92°C).

The total COP-(c+h) of 5,0 is achieved.

The first plants have been delivered this year.

### SPECIAL THANK-WORD.

For Mr.Lucas, the contractor AXIMA REFRIGERATION from France, who installed the CO<sub>2</sub>/NH<sub>3</sub> cascade plant for bakery products and gave us access to all details of this heat pump plant.